RECORD 6 300 AREA 925 S.A. N.G. 158 CLASSIFIED FILES SEGREGATION OF FLUORIDE SLUDGE EUILDING 313 \$40,000 ⊕ ⊕: LE LEBERT BELLEVILLE lipon authorization of formal $(\mathcal{M}_{\mathcal{T}})$ project proposal 12 months after authorization 2 B1 400 A (2000) DA E& 19 menths after nuthorization **DECLASSIFIED** BY CG-NMP-2 SEPT. 2000 AND APPROVED FOR **PUBLIC RELEASE** B840 NAME/DATE /// NAME/DATE PNNE NSAN ADD'S --- J.=-

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REASON SHEET

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1. Present Facilities and to What Extent They are Inadequate

The 300 krea fabrication process in which shugs are prepared for the in the piles produces some scraparanium sats (60 chaining of remium precipitated from nitricencid and also from hydrofluoric acid. The skifting system involves a procedure in which the rejected chars are first immersed in caustic to dissolve the outer cans, then in 20% hydrogen-fluoride to dissolve the bond, and then in nitric acid to "pickle" or dissolve thin layer of the uranium surface. The sludge from each of these dissolving processes is then pumped to a common neutralizing tank after which the granium salts are recovered by filtration and shaped off-sate for purification and reduction to the metal. The studge from the caustic and nitric acid dissolving, which amounts to about 9% of the wholes is of such curity that the off-plant purification operation for it could be eliminated and the metallic phase regenerated directly. However, the sludge from the hydrogen-fluoride dissolving, amounting to about 1%, contaminates the whole with fluoring making the costly purification step necessary for the entire batch.

2. Description of Proposed Work

It is proposed that separate facilities be provided for the recovery of 6 (fluoride sludge) from the hydrofluoric acid solution used in the slug recovery operation. This will consist of disconnecting the hydrofluoric acid tank drain piping from the rest of the drain system to the existing neutralizing tank and the installation of one additional smaller neutralizing tank, pumps, filters, incidental piping and facilities for the hydrofluoric acid only.

Additional incident space will be required to house this additional equipment.

3. Advantages to be Cained and Justification for Proposed Work

The cost of purifying the C-6 sludge prior to the regeneration of the uranium metal is estimated at approximately \$3.50 per pound. At the current DECLASSIFIED

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rate of production, if 99% of the C-6gsludge could be eliminated from the purification operation, a saving of approximately \$46,000 per year would result.

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4. Why Existing Facilities Cannot be Utilized

There are no existing facilities to accomplish the proposed operation changes.

5. Time Required to Accomplish Work After Authorization

It is estimated that the proposed installations will be ready for use 12 months after authorization and all work physically completed in 18 months.

6. Funds

A budgetary allotment of \$40,000 to be required in fiscal year 1950 and \$8,000 in fiscal year 1951.

A formal project proposal is to be submitted at a later date.

7. Remarks

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This preliminary project was prepared by the Project Engineering Division at the request of the "P" Division.